Controlling NO\(_x\) Emission from Post-blast Process Gases

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Abstract

This study investigates effect of the pH on nitric oxides (NO\(_x\)) removal. A spray tower has been used to study the absorption of nitrogen oxides in both acidic and alkaline solution of sodium chlorite (NaClO\(_2\)). Sodium chlorite was used as an oxidant in order to oxidise NO to NO\(_2\), which is highly soluble in aqueous phase. NO was oxidized to NO\(_2\) followed by NO\(_2\) and ClO\(_2\) to ClO\(_2\)\(^-\) in liquid phase respectively. The latter was found to be reduced to Cl\(^-\) and ClO\(^-\). Varying pH of the solution form acidic and alkaline phases, pH (4-12), which is influential in the efficiency of NO\(_x\) removal, was studied. According to the experiments carried out in this study, alkaline medium was found to be more reliable than acidic one, and 100% NO with 86% NO\(_x\) removal was observed in ambient conditions. The main reason is attributed to hydrolysis of N\(_2\)O\(_4\) in higher pH (basic). Experimental results demonstrate the feasibility of the aqueous solution of sodium chlorite for NO\(_x\) removal.

Keywords: NO\(_x\) removal, Sodium chlorite (NaClO\(_2\)), acidity, alkalinity, FT-IR

Introduction

Emission of NO\(_x\) has been a main concern for environment owing to its destructive effects (acidic rain e.g.,) on human being, for example, respiratory system and ecosystems [1]. NO\(_x\) is mainly attributed to nitric oxide (NO); however, there are other constituents in NO\(_x\) such as nitric dioxide (NO\(_2\)), and small quantities of N\(_2\)O\(_4\) and N\(_2\)O\(_3\) due to equilibrium reactions between NO and NO\(_2\). Having said that NO has deteriorating properties on ecosystems, it also contributes in nutrient overload, toxic chemicals production, and global warming [2]. Moreover, NO\(_x\) is one of the main ingredients involved in the formation of urban smog, ground-level ozone leading to eutrophication and heart disease; which is why, controlling of NO and NO\(_2\) have come to a sharp focus currently [3]. Nitrogen Oxide (NO) is formed when a fuel is burnt at high temperature, as a combustion process. Road transportation accounts for 61% of NO emission, while industrial activities such as mining, motor vehicles, and electric utilities make up 32% of the pollution. Typically, NO\(_x\) is emitted as NO up to 90-95% by volume; meanwhile, 5-10% of the remaining emits as NO\(_2\). NO is an odourless and colourless gas, therefore, NO\(_2\) causes NO\(_x\) to become visible as a pungent reddish-brown gas [4]. Fig.1 shows how the NO\(_x\) gas look like after detonation.
In this study, our focus will be on other source of NO\textsubscript{x}, which is emitted after explosive detonation in mining fields; in other words, NO is oxidized to NO\textsubscript{2} and solubility of NO\textsubscript{x} increases due to formation of N\textsubscript{2}O\textsubscript{3} and N\textsubscript{2}O\textsubscript{4}; therefore, an oxidant is required to oxidize and absorb NO. Finally, nitrogen oxide is oxidised to nitrite and nitrate depending on composition of the solution. Open-cut coal mining is a widespread technique in countries like Australia and following that a universal explosive called ammonium nitrate/fuel oil (ANFO) is used for this purpose. In recent years, huge attentions have been drawn to the controlling and monitoring of NO/NO\textsubscript{2} on the basis of the adoption of the Clean Air Act in 1970 due to 20\% increase of NO. Therefore, inexpensive and efficient removal techniques were introduced. In other words, selective catalytic reduction (SCR), selective noncatalytic reduction (SNCR), flue gas recirculation (FGR), and thermal treatments are amongst them. All these technologies have some disadvantages and capital costs, high temperatures, and disposal problems are to name but a few [3]. In fact, NOx removal can be divided in two parts which are dry reduction process and wet methods. SCR and SNCR are considered as dry methods, whereas, wet scrubbing absorption, electron beam irradiation or plasma and so on are categorized as wet methods. Amongst the technologies mentioned above, it has been proven that wet scrubbing is the most promising, inexpensive, and efficient removal technique [5]. Wet scrubbing absorption can easily dissolve NO\textsubscript{2} in an aqueous phase, but there is a problem with NO whose solubility in aqueous phase is very low; in other words, liquid-phase resistance to mass transfer is sharply increased [1, 6]. In order to overcome this problem, the aqueous phase must contain a strong oxidant which is able to convert NO to NO\textsubscript{2} that is soluble in the aqueous phase. There are known strong oxidants such as hydrogen peroxide (H\textsubscript{2}O\textsubscript{2}) and peracids, yellow phosphorus (P\textsubscript{4}), organic hydroperoxides, sodium chlorite (NaClO\textsubscript{2}), potassium permanganate (KMnO\textsubscript{4}), sodium hypochlorite, peroxymonosulfate (oxone), and Sodium persulfate (Na\textsubscript{2}S\textsubscript{2}O\textsubscript{8}) [3]. Having said the available technologies, counter current packed bed scrubbers, spray towers, ejector venturi scrubbers, plate columns, mist scrubbers and even mobile-bed absorbers are used in gas absorption-oxidation techniques [7]. Since this research deals with controlling and capturing NO\textsubscript{x} which is emitted and drifted after blast in mining area, mist scrubber or spray towers are categorized in this project. Wet scrubbing has been discouraged by industries in spite of its advantages over other techniques; in other words, cost of chemicals is high along with
their disposal solutions. Therefore, an inexpensive, efficient and environmentally benign chemical should be suggested. Sodium chlorite (NaClO₂) could be one of reliable oxidant used in NOₓ removal because it is not only inexpensive but also is stable and its application has already been reported[8]. Also, the absorption of NOₓ in NaClO₂ was studied by Sada et.al in their seventies [9-11]. They carried out a series of kinetic investigations in a bubble-column reactor using sodium chlorite. They proved that oxidation power of NaClO₂ rose with decrees in pH value; meanwhile, NO₂ may desorb from the solution if OH⁻ amount is low. In order to avoid this to happen, additional OH⁻ is required to fix NO₂ as NO₃⁻ [8]. The flowing reaction occurs once OH⁻ is added.

\[
4\text{NO} + 3\text{ClO}_2^- + 4\text{OH}^- \rightarrow 4\text{NO}_3^- + 3\text{Cl}^- + 2\text{H}_2\text{O} \quad (1)
\]

On the top that, other researchers have published their research results which have been summarized in Table 1[8].

<table>
<thead>
<tr>
<th>Experiment</th>
<th>Reactor Type</th>
<th>[NaClO₂] (M); [NaOH] (M)</th>
<th>pNOₓ (ppm)</th>
<th>pH</th>
<th>Gas-liquid contact time (s)</th>
<th>NOₓ removal efficiency (%)</th>
<th>Temperature (°C)</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>packed</td>
<td>0.05-0.67</td>
<td>200-900</td>
<td>-</td>
<td>9-18.5</td>
<td>&lt;70</td>
<td>ambient</td>
</tr>
<tr>
<td>2</td>
<td>bubble</td>
<td>0.008-0.08</td>
<td>2000</td>
<td>10-14</td>
<td>60</td>
<td>&lt;100</td>
<td>ambient</td>
</tr>
<tr>
<td>3</td>
<td>Spray packed</td>
<td>0.037-0.15, 0.008-0.08</td>
<td>300-2000</td>
<td>6.5-12.9</td>
<td>-</td>
<td>&lt;95</td>
<td>ambient</td>
</tr>
<tr>
<td>4</td>
<td>packed</td>
<td>0.0-0.6</td>
<td>290</td>
<td>8-12</td>
<td>11.8</td>
<td>51-84</td>
<td>ambient</td>
</tr>
<tr>
<td>5</td>
<td>packed</td>
<td>0.05-0.2; 0-1.0</td>
<td>200-1000</td>
<td>4.5-9.5</td>
<td>1</td>
<td>15.9-61.5</td>
<td>ambient</td>
</tr>
<tr>
<td>6</td>
<td>Sieve Tray</td>
<td>0.0008-0.0035</td>
<td>200-800</td>
<td>4-6</td>
<td>1</td>
<td>36.6-71.9</td>
<td>ambient</td>
</tr>
</tbody>
</table>

Seda et.al [9] proved that absorption of nitric oxides occurs in a fast reaction regime. In fact, rate constant for the reaction (1) was empirically correlated as follows:

\[
k_{mn} = 3.8 \exp (-3.73[\text{NaOH}]) \quad (2)
\]

Where, OH⁻ concentration should be in the range of, 0.05<[NaOH]<0.5 kmol/m³[9]. Brogren et.al discovered that pH value of solution had a significant impact on the absorption efficiency. It can be explained that major fraction of nitric oxides was absorbed via hydrolysis of N₂O₃ and N₂O₄ [12]. They also suggested reaction (3) as the reaction between NO₂ and ClO₂ solution.

\[
4\text{NO}_2^- + \text{ClO}_2^- + 4\text{OH}^- \rightarrow 4\text{NO}_3^- + \text{Cl}^- + 2\text{H}_2\text{O} \quad (3)
\]

Acidic medium has also been reported a lot in literature so that some researchers called it better that of alkaline. Deshwal et.al has investigated application of acidic NaClO₂ and has shown that it performed better comparing to alkaline one [13]. It is said that chlorine dioxide gas released from decomposition of sodium chlorite in acidic medium as shown in reaction (4). Plus, it performs as an oxidant, which increases the oxidation of NO in the gas phase[14].

\[
4\text{ClO}_2^- + 2\text{H}^+ \rightarrow 2\text{ClO}_3^- + \text{Cl}^- + \text{H}_2\text{O} \quad (4)
\]

They also assert that oxidative ability of sodium chlorite decreases as pH of solution increases; while, absorptive ability of NaClO₂ increased in alkaline solution [15]. Despite a lot of studies on NO removal in both either acidic medium or alkaline one, this study focuses on impact of various pH
values in ClO₂ and NO₂ formation; moreover, identification and qualification of compounds were discussed. This study is the first one which demonstrates that alkaline medium has more advantages over acidic one with regards to NOₓ removal as well as NO₂ and ClO₂ formation. In the meantime, chemistry of reactions was briefly discussed.

**Experimental section**

Fig. 2. shows a schematic diagram of the novel wet scrubber which has been developed for NOₓ removal. The spray tower consists of a chamber, a cylindrical chamber, as well as a nebuliser. In other words, nebuliser produces very fine droplets whose size is less than 10µm; which means that, process gasses have huge chances to contact the solution. The experimental section is divided to three parts: NOₓ gas simulation system, the spray chamber, and reaction product sampling and analysing system. Nitric oxides were obtained from a NOₓ cylinder and metered through a mass flow controller (MFC). Nitrogen gas was also applied in order to dilute the mainstream gas (NOₓ) as well as production of small droplets by nebuliser. Flow rates of both gasses vary between 0.9-1.1 L/min. Next part considered as absorption chamber in which NO was oxidized and absorbed into the aqueous solution. It performs in the way that those gasses continuously flowed through the system; while, effluent was collected at the bottom of the reactor. Oxidant or liquid solution was pumped upward along with nitrogen gasses through nebuliser. There is reflux glassware at the top of the reactor, which ensured that no liquid passes through the chamber. Furthermore, a Nafion dryer was embedded after the reflux glassware to ensure that all moisture of gas has been removed this was done to protect the gas analyser. Inlet and outlet concentration of NO was measured by 42i-TL TRACE Level NOx Analyzer (Thermo Fisher Scientific Inc.)

The SeaSpray concentric nebulizer (Glass Expansion) was used in this experiment to produce fine droplets. The feature of the device was depicted in Fig. 3.
The whole procedures can be described in a simple explanation. In fact, gas stream containing NOx/N2 was flowed into the spray chamber, therefore, gas flow rates can be varied during the experiment to meet mist production requirement. It is normally 1L/min based on nebulizer specification. Once mist was produced, it contacted with the toxic gas and oxidation-absorption process commenced. The idea by which mists were formed, was because of having huge surface area which caused quick and efficient oxidation-absorption process. In other words, small droplet were moving upward while contacting toxic gas could be influenced by inertial impaction, direct interception as well as Brownian diffusion[16]. This means that significant gas-liquid interfacial area was obtained, which resulted in low consumption of oxidant as well as low waste formation. Ultimately, each experiment took almost 15-20 min and majority of nitric oxides removal occurs in seconds since it is in the fast reaction regime. Nebulizer mists up the solution upward and oxidation-absorption occurred resulting in 100% -86% removal of NO and NOx respectively. pH played a key role in this study, therefore, all experiments were carried out using buffers which caused the pH remained constant throughout the whole process. Boric acid, phosphate, sodium bicarbonate and acetic acid were used as buffers in the wet spraying medium. This study mainly encompasses the effect of various pH on nitric oxides removal.

Results and discussion

Acidic medium

In acidic medium, where pH is low, chlorine dioxide (ClO2) is formed. ClO2 formation could be attributed to decomposition of NaClO2 solution. Reaction (5) demonstrates ClO2 formation [17].
5ClO₂ + 4H⁺ → 4ClO₂ + Cl⁻ + 2H₂O  \hspace{1cm} (5)

ClO₂ is a strong oxidant that can react with NO and oxidise it to NO₂, which is highly soluble in water. Reaction (6) shows how NO gets oxidised to NO₃ by ClO₂. One of the ways to detect chlorine dioxide is to check the colour of the solution. Once the colour turned to greenish-yellow, it can be confirmed that ClO₂ exists in the solution [6].

5NO + 3ClO₂ + 4H₂O → 5HNO₃ + 3HCl  \hspace{1cm} (6)

In order to find dominant reaction, pH value and chlorite concentration play a key role in oxidation-absorption process. In acidic medium oxidative ability of NaClO₂ solution is powerful and converts NO to NO₂ [17]. In our experiment, buffer solutions were used in order to keep the pH level constant [18]. Experiments were carried out in the range of 3<pH<7 to check the NOx removal. According to the experimental section, 470 ppm NOₓ entered the spray chamber with 1L/min flow rate and contacted NaClO₂ solution at pH=4±0.2, as a result, 72% of NOₓ was removed. It should be noted that this removal procedure has also leaded to desorption of NO₂ from NaClO₂ solution. In other words, NO₂ increased and desorbed to gas phase owing to its saturation in liquid phase. This pH cannot be optimum since NO₂ level rose almost 5 times more that inlet which was 20 ppm. Fig.4. depicts that NO₂ increased; while, NO has reached zero. For this experiment, (sodium acetate, acetic acid) was used as a buffer solution. Another experiment was conducted at pH=6 with phosphate buffer (Na₂HPO₄, NaH₂PO₄) and the result was almost similar to that of pH=4. In fact, 78% of NOₓ removed; while, NO₂ concentration reached a high level, which is unacceptable. Powerful oxidative ability and poor absorption state could be the reason of low efficiency as well as high NO₂ desorption. Moreover, in acidic state there is no hydrolysis of N₂O₃ and N₂O₄ which result in absorption of NO₂. Considering that this study investigates the optimum pH at which NO and NO₂ get removed, we must find a way to control ClO₂ formation. Acidic medium cannot be the solution; however, oxidation ability is high in acidic state. In other words, controlling of NO₂ formation along with ClO₂ was the agenda of this study. Since our experiments have been simulated as to they are in a condition in which a post-blast gases are present, acidic solution of NaClO₂ not only desorb NO₂ but also forms ClO₂ which is hazardous for the environment. Therefore, alkaline solution of NaClO₂ was employed to assist us removing NO₂ as well as ClO₂ to the best of its ability. Fig.6. obtained by FT-IR shows that a great amount of ClO₂ was formed during the experiment in acidic medium.
Alkaline medium

Having discussed NO removal using acidic solution of NaClO₂, alkaline medium should be considered. The beauty of alkaline reaction is when NO₂ reacts with chlorite and nitrate (NO₃⁻) is produced. The following reaction can be considered NO₂ reaction with ClO₂⁻:

\[
4\text{NO}_2 + \text{ClO}_2^- + 4\text{OH}^- \rightarrow 4\text{NO}_3^- + \text{Cl}^- + 2\text{H}_2\text{O} \quad (7)
\]

Hydrolysis reaction of NO₂ plays a key role along with above reaction. As it was described earlier, ClO₂⁻ formation should be avoided; however, there is no decomposition of NaClO₂ solution since it only occurs in acidic condition. It should be noted that hypochlorite was formed and reacted with chlorite ion to produce ClO₂, which is an undesirable product although it has powerful oxidative ability. Reaction (8) can be considered to be:

\[
2\text{ClO}_2^- + \text{HOCl} \rightarrow 2\text{ClO}_2^- + \text{Cl}^- + \text{OH}^- \quad (8)
\]

Hypochlorite ion (ClO⁻) is said to be produced at pH 7-10, however, it was not detected by chromatography due to low conductivity[12]. Reaction (8) occurs when pH drops below 10; therefore, buffer was used to keep pH constant over the course of the reaction. There is also an alternative to suppress ClO₂⁻ formation which can be justified by the following reaction.

\[
\text{ClO}^- + \text{H}_2\text{O} \rightarrow \text{Cl}^- + \text{H}_2\text{O} + \text{O}_2 \quad (9)
\]

Reaction (9) is applicable for the reaction occurring when pH value drops below 7. Given the importance of mitigation of toxic gases such as NO₂ and ClO₂, it was proven that alkaline solution
works much better than acidic solution with strong oxidative ability. Fig. 5.1. shows how much NOx is removed over the course of experiment. Fig. 5.2. depicts that a very negligible amount of ClO$_2$ is formed once alkaline solution is applied. Whereas, Fig. 6. Shows how acidity can affect the process by producing huge amount of ClO$_2$.

![Graph showing NOx removal in acidic condition, pH>11](image1)

**Figure.5.1. NO$_x$ removal graph in acidic condition, pH>11**

![Spectra of gaseous at pH value>12 compounds obtained by FT-IR](image2)

**Figure.5.2 Spectra of gaseous at pH value>12 compounds obtained by FT-IR**
Figure 6. Spectra of gaseous at pH value <4 compounds obtained by FT-IR

**Conclusions**

Results of this study demonstrate that alkaline NaClO₂ solution has more advantages than acidic one. It showed that 100% removal of NO was observed with 86% NO₂ removal containing NO₂, plus, a buffered solution of NaClO₂ demonstrated higher absorption and stability; moreover, a negligible amount of ClO₂ was formed when pH >11. Optimal NO and NO₂ absorption was found to be at pH value >11 due to having low concentration of ClO₂ in the gas phase.

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**References:**